

## MODELLING OF THE THERMOPHYSICAL PROPERTIES OF CITRIC ACID AQUEOUS SOLUTIONS. DENSITY AND VISCOSITY

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### Abstract

Citric acid is an organic acid produced by carbohydrates fermentation process under microorganisms' action. Its uses in a large variety of fields going from food products to cosmetics and medicines require a good knowledge of its industrial behavior. From this point of view, thermo-physical properties (density, viscosity, thermal heat capacity, thermal conductivity and so on) present a major interest. As consequence, in this paper, different mathematical relations between temperature and concentration and density and dynamic viscosity of aqueous solutions made of anhydrous citric acid were established. The known data were fitted in different equations in order to assess and select suitable mathematical models. Their accuracy was studied using several statistical analysis tools such as correlation coefficient, ANOVA test, relative error etc. Taking into consideration the level of precision and the simplicity of formulation, several equations were generated for each of the studied thermo-physical property. For density proposed model the correlation coefficient  $R^2$  is 0.999 and the average relative errors is 0.03% (absolute value). The dynamic viscosity equation was based on the Arrhenius model with average relative errors of 0.59% (absolute value). All the obtained equations can be uploaded in computer software available both for industrial and academic users and successfully used to facilitate the sizing and the optimization calculations of various technological processes and equipment.

**Keywords:** citric acid, thermo-physical properties, mathematical modeling.

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### 1. INTRODUCTION

Citric acid is a common metabolite of plants and animals (Angumeenal A.R. and Venkappayya D, 2013). It dominates the category of organic acids, with a global production estimated in 2007 at more than 1.6 million of tons (Berovic M. and Legisa M., 2007). Many different studies were realized in order to assess the appropriate conditions for citric acid production. The world's existing demand is almost entirely (over 99%) met by fermentative technologies (Dhillon, G.S. et al, 2011). The microbial process for production of a high volumes of the aforementioned metabolite is based especially on the use of filamentous fungus *Aspergillus niger* (Sauer M. et al, 2008, El-Abyad M.S. et al, 1992, Saha M.L. and Takahashi F., 1997) in submerged (Paul G.C., et al, 1999, Papagianni M. and Matthey M., 2004) or static (Berovic M. and Legisa M., 2007) liquid cultures but other

microorganisms such *Yarrowia lipolytica* (Papanikolaou S., 2008) can also conduct to remarkable quantities of this acid. However, its production requires high energy consumption and expensive raw materials. These aspects led to the search of alternative low cost substrates. In recent years, considerable interest has been focused on agro-industrial wastes knowing that this direction serves also to solve waste management problem faced by agro-industries. Moreover, industries will be benefitted by extra revenue from the value addition of wastes. Thus, different types of substrates were successfully employed for microorganisms' development. Dhillon et al, 2011, shown that the apple pomace ultrafiltration sludge presents a promising potential for the production of citric acid by *Aspergillus niger*. Imandi et al, 2008, study involved the use of statistical experimental designs to optimize medium constituents of the fermentation process for the production of

citric acid from pineapple waste. The use of lignocellulosic materials available in agricultural wastes as a source of raw material for citric acid production (Khosravi-Darani K. and Zoghi A, 2008, Kumar D. et al, 2003) is also of considerable interest because of their renewable nature and abundance. Various other materials such as wastes from fruits processing industry (Kumar D. et al, 2003, Sassi G. et al, 1991) or molasses (El-Abyad M.S. et al, 1992, Jianlong, W. et al, 2000) have been also subjected to specific treatments able to conduct to citric acid.

Once obtained, the citric acid has a broad range of versatile applications, e.g. in food (as acidifying and flavor-enhancing agent, for the extraction of pectin from citrus peel (Kurita O. et al, 2008), or from cacao pod husks (Vriesmann L.C. et al, 2012), in combination with high-intensity pulsed electric fields for non-thermal pasteurization of fruit juices (Mosqueda-Melgar J. et al, 2008), in combination with CO<sub>2</sub> for the development of new packaging methods for fish storage (Schirmer B.C. et al, 2009)), in pharmaceuticals and cosmetics (for the production of inhalers for smoking cessation (Behm F.M. et al, 1993), to prolong the in vivo gastro-retention of a floating dosage form in the fasted state (Stops F. et al, 2006), as a release-modifying agent in melt extruded matrix tablets (Schilling S.U. et al, 2008), in combination with chitosan for the development

of calcium phosphate cement for bone substitute materials (Yokoyama A. et al, 2002)). It is involved also in many advanced domains such as: biomedicine (for the production of biopolymers for culturing a variety of human cell lines (Vieira M.G.A. et al, 2011), nanotechnology (for the production of nanocomposites (Chung E.J. et al, 2011)), agriculture (for processes of bioremediation of heavy metals due to its powerful sequestering action with various transitional metals (Chen Y.X. et al, 2003)) or chemical industry (for the production or improvement of catalysts (Ibeh B. et al, 2009, Rinaldi N. et al, 2010, Li H. et al, 2011)). Small quantities of citric acid are employed in silvering and engraving and in dyeing and calico printing (Angumeenal A.R. and Venkappayya D, 2013).

In order to commercially produce this valuable microbial product and to use it in an effective and economically way in so many different areas of interest it is necessary to know how its thermophysical properties evolve. As we have shown in other of our researches (<sup>a</sup>Simion A. I. et al, 2011, <sup>b</sup>Simion A. I. et al, 2011, <sup>c</sup>Simion A. I. et al, 2011) previously published this type of properties can be illustrated by various relations. Thus, this paper focuses on the study of citric acid aqueous solutions density and viscosity. Their evolution when influenced by parameters such as temperature and concentration was analyzed.

**Table 1.** Variation of citric acid aqueous solutions density with temperature and citric acid content (Kharat S. J., 2008)

Citric acid concentration, C [% w/w]	Density, $\rho$ [kg·m <sup>-3</sup> ]			
	Temperature, T [K]			
	298.15	303.15	308.15	313.15
0	997.00	995.60	994.00	992.20
6.43	1022.5	1020.9	1019.1	1017.1
9.94	1035.3	1033.6	1031.7	1029.7
16.99	1059.4	1057.6	1055.5	1053.4
19.82	1068.5	1066.6	1064.5	1062.3
25.18	1085.0	1083.0	1080.7	1078.5
30.00	1099.0	1096.8	1094.5	1092.2
34.00	1110.1	1107.8	1105.3	1103.1
39.94	1125.7	1123.3	1120.7	1118.5
44.99	1138.3	1135.8	1133.1	1130.9

**Table 2.** Variation of citric acid aqueous solutions dynamic viscosity with temperature and citric acid content (Kharat S. J., 2008)

Citric acid concentration, <i>C</i> [% w/w]	Dynamic viscosity, $\mu \cdot 10^3$ [Pa·s]			
	Temperature, <i>T</i> [K]			
	298.15	303.15	308.15	313.15
0	0.894	0.800	0.722	0.658
6.43	1.045	0.920	0.813	0.725
9.94	1.118	0.985	0.869	0.772
16.99	1.280	1.131	1.002	0.885
19.82	1.365	1.205	1.068	0.943
25.18	1.532	1.345	1.193	1.059
30.00	1.693	1.482	1.331	1.179
34.00	1.843	1.631	1.445	1.275
39.94	2.122	1.857	1.632	1.454
44.99	2.432	2.120	1.825	1.613

Our work was aimed to develop mathematical models able to describe the above mentioned thermophysical properties of citric acid and to compare them with the experimental data presented in literature. The developed models were verified using the relative error, ANOVA analysis and correlation coefficient. The obtained results showed good level of agreement for the proposed equations.

## 2. EXPERIMENTAL

Tabular data provided by the technical and scientific publications (Tables 1 and 2) concerning the variation of aqueous citric acid solutions density and dynamic viscosity with concentration and temperature were used as primary data for the regression analysis. For simple data integration, plotting and ANOVA analysis the Microsoft Excel™ 2007 spreadsheets was used. ANOVA analysis tool is able to offer more precise information between existing data and the predicted values obtained by the proposed mathematical models. For more complex and atypical data plotting in 2D (“vapor pressure” model, “heat capacity” model etc.) the CurveExpert® software was employed. The representation of tabular data in 3D as a surface response was fitted and analyzed in TableCurve 3D® v.4 software. The experimental data were plotted in *Temperature – Thermo-physical property, Citric acid concentration in aqueous solutions – Thermo-*

*physical property* coordinates and different types of regression techniques, involving the method of least squares, relative error  $\varepsilon$  (Equation 1) and ANOVA were used to reveal the best-fit equation.

$$\varepsilon = \left| \frac{\text{Data}_{\text{tabular}} - \text{Data}_{\text{calculated}}}{\text{Data}_{\text{calculated}}} \right| \cdot 100[\%] \quad (1)$$

## 3. RESULTS AND DISCUSSIONS

### Density

Using Microsoft Excel™ 2007 spreadsheets and CurveExpert® software, 10 linear correlations (taking in consideration the best fit and simplicity in formulation) between temperature *T*, [K] and density  $\rho$  [kg·m<sup>-3</sup>], at constant citric acid concentrations *C* [% w/w] have been established:

$$\rho = a_1 + a_2 T \quad (2)$$

The  $a_1$  and  $a_2$  values are presented in Table 3. The regression coefficients  $R^2$  are greater than 0.99, thus indicating a good correlation of variables. In order to correlate  $a_1$  and  $a_2$  coefficients with concentration *C*, [% w/w], different models were used in CurveExpert® software (1<sup>st</sup>, 2<sup>nd</sup> and 3<sup>rd</sup> degree polynomial equations, “vapor pressure” model, “heat capacity” model, etc.).

**Table 3.** Coefficients for equation no. 2

Citric acid concentration, $C$ [% w/w]	Equation 2 coefficients		
	$a_1$	$a_2$	$R^2$
0	1092.5	-0.320	0.9985
6.43	1129.9	-0.360	0.9990
9.94	1146.9	-0.374	0.9995
16.99	1179.3	-0.402	0.9999
19.82	1192.0	-0.414	0.9992
25.18	1215.1	-0.436	0.9989
30.00	1234.4	-0.454	0.9987
34.00	1250.2	-0.470	0.9987
39.94	1270.0	-0.484	0.9975
44.99	1286.7	-0.498	0.9969

The best fit model is the quadratic equation with good regression coefficients (Table 4).

$$\text{Coefficient } t = b_1 + b_2T + b_3T^2 \quad (3)$$

Combining the equations 2 and 3 and replacing the coefficients with numeric values, the final form of proposed equation model becomes (Equation 4):

$$\rho = (1093.8 + 5.53238 \cdot C - 0.02784 \cdot C^2) + (-0.3226 - 0.005345 \cdot C + 0.0000328 \cdot C^2) \cdot T \quad (4)$$

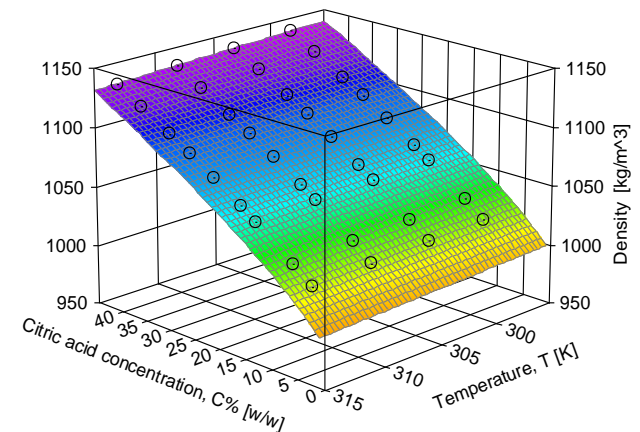
Using the relative error equation, the calculated data given by the density mathematical model and the existing tabular data were compared (Table 5) obtaining a final average of 0.03% (absolute value). The ANOVA analysis (Table 6) was used to compare the values of density tabular and calculated data at 10 different concentrations in 4 temperatures variation.

The results presented in Table 6 showed that the sample  $P$ -value is 0.975118 greater than the targeted alpha 0.05 and the  $F$  crit value is larger than the  $F$ -test one. The null hypothesis is not rejected indicating that is not a statistical difference between tabular and calculated data.

By plotting tabular data for aqueous citric acid solutions in TableCurve 3D® v.4 software (Figure 1) an equation for the response function was generated, chosen due to the accuracy and simplicity of formulation.

The Equation 5 is a simple equation, Rank 1, Eqn. 151232557 in TableCurve 3D® v.4 library, with a precision of  $R^2 = 0.999982817$ , FitSdErr = 0.38247068, Fstat. = 257528.25. The coefficients values are presented in Table 7.

$$\ln \rho = a_1 + a_2 \cdot C^{(0.5)} \ln C + a_3 \cdot T^3 \quad (5)$$



**Figure 1.** Citric acid aqueous solutions density values plotted in TableCurve 3D and fitted with simple equation type (Equation 5) with residuals

**Table 4.** Coefficients for equation no. 3

Equation 2 coefficients	Equation 3 coefficients			
	$b_1$	$b_2$	$b_3$	$R^2$
$a_1$	1093.8	5.53238	-0.02784	0.9998
$a_2$	-0.3226	-0.005345	0.0000328	0.9985

**Table 5.** For densities of citric acid aqueous solutions the absolute value of relative errors for calculated data versus tabular data

Citric acid concentration, C [% w/w]	Density, $\rho$ [kg·m <sup>-3</sup> ]												
	Temperature, T [K]												
	298.15			$\epsilon$ , %	303.15		$\epsilon$ , %	308.15		$\epsilon$ , %	313.15		$\epsilon$ , %
	TD*	CD*			TD	CD			TD		CD		
0	997.00	997.80	0.08	995.60	996.20	0.05	994.00	994.60	0.05	992.20	993.00	0.07	
6.43	1022.5	1022.4	0.01	1020.9	1020.6	0.02	1019.1	1018.8	0.02	1017.1	1017.1	0.00	
9.94	1035.3	1035.2	0.01	1033.6	1033.3	0.02	1031.7	1031.4	0.02	1029.7	1029.6	0.01	
16.99	1059.4	1059.5	0.01	1057.6	1057.5	0.01	1055.5	1055.5	0.00	1053.4	1053.5	0.00	
19.82	1068.5	1068.8	0.02	1066.6	1066.7	0.00	1064.5	1064.6	0.01	1062.3	1062.5	0.02	
25.18	1085.0	1085.5	0.04	1083.0	1083.3	0.03	1080.7	1081.2	0.04	1078.5	1079.0	0.04	
30.00	1099.0	1099.7	0.06	1096.8	1097.4	0.05	1094.5	1095.2	0.06	1092.2	1092.9	0.06	
34.00	1110.1	1110.8	0.06	1107.8	1108.5	0.06	1105.3	1106.2	0.07	1103.1	1103.8	0.06	
39.94	1125.7	1126.3	0.05	1123.3	1123.9	0.05	1120.7	1121.5	0.06	1118.5	1119.1	0.04	
44.99	1138.3	1138.4	0.01	1135.8	1136.0	0.01	1133.1	1133.5	0.03	1130.9	1131.0	0.00	
	Average $\epsilon$ , %		0.03	Average $\epsilon$ , %		0.03	Average $\epsilon$ , %		0.03	Average $\epsilon$ , %		0.03	

\* TD – tabular data, CD – calculated data

**Table 6.** The ANOVA test summary

SUMMARY	Temperature, T [K]				Total	
	298.15	303.15	308.15	313.15		
<i>Tabular data</i>						
Count	10	10	10	10	40	
Sum	10740.8	10721	10699.1	10677.9	42838.8	
Average	1074.08	1072.1	1069.91	1067.79	1070.97	
Variance	2130.986	2097.662	2065.228	2053.679	1932.047	
<i>Calculated data</i>						
Count	10	10	10	10	40	
Sum	10744.41	10723.4	10702.4	10681.39	42851.61	
Average	1074.441	1072.34	1070.24	1068.139	1071.29	
Variance	2139.427	2112.978	2086.694	2060.575	1944.043	
ANOVA						
<i>Source of Variation</i>	<i>SS*</i>	<i>df*</i>	<i>MS*</i>	<i>F</i>	<i>P-value*</i>	<i>F crit</i>
Sample	2.050654	1	2.050654	0.00098	0.975118	3.973897
Columns	442.4069	3	147.469	0.070445	0.97555	2.731807
Interaction	0.044861	3	0.014954	7.14E-06	1	2.731807
Within	150725.1	72	2093.404			

\* SS – sum of squares, df – degrees of freedom, MS – mean square, P-value – level of significance

**Table 7.** Coefficients for equation no. 5

Coefficient	Equation 5 coefficients			R <sup>2</sup>
	a <sub>1</sub>	a <sub>2</sub>	a <sub>3</sub>	
Value	6.9429198	0.0051584066	-1.40881576e-0.9	0.9999



### Dynamic viscosity

The most common mathematical model, in literature, for calculating the viscosity is based on the equation of Arrhenius because it creates a good correlation between experimental data and calculated values.

$$\mu = \mu_0 \cdot e^{-\frac{E_a}{R \cdot T}} \quad (6)$$

where:  $\mu$  – dynamic viscosity [Pa·s],  $\mu_0$  – water dynamic viscosity [Pa·s],  $E_a$  – activation energy [kcal·mol<sup>-1</sup>],  $R$  – universal gas constant [1.987·10<sup>-3</sup> kcal·mol<sup>-1</sup>·K<sup>-1</sup>],  $T$  – absolute temperature [K].

Taking logs of equation (6), it gets (7):

$$\log \mu = \log \mu_0 - \frac{E_a}{2.303 \cdot R} \cdot \frac{1}{T} \quad (7)$$

and:

$$\frac{E_a}{R} = 2.303(\log \mu_0 - \log \mu) \cdot T \quad (8)$$

By plotting the results obtained from Equation 8 in TableCurve 3D® v.4 software (Figure 2) an equation for the response surface was generated (Equation 9). It correlates tabular data from Table 1 and water viscosity.

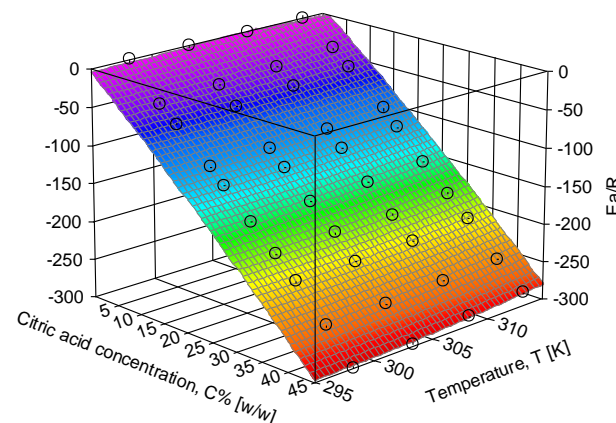
The Equation 9 is a polynomial equation, Rank 17, Eqn. 301 in TableCurve 3D® v.4 library with a precision of  $R^2 = 0.99939759$ , FitSdErr = 2.4040784, Fstat. = 11281.2.

$$\frac{E_a}{R} = a_1 + a_2 \cdot C + a_3 \cdot T + a_4 \cdot C^2 + a_5 \cdot T^2 + a_6 \cdot C \cdot T \quad (9)$$

Combining the equations 6 and 9 and replacing the coefficients with numeric values, the final

form of the proposed equation model is (Equation 10):

$$\mu = \mu_0 \cdot e^{\frac{(2803.92257 - 7.3756887C\% - 19.001965T - 0.014509371C\%^2 + 0.032140717T^2 + 0.0052423574T \cdot C\%)}{T}} \quad (10)$$



**Figure 2.**  $E_a/R$  values plotted in TableCurve 3D and fitted with polynomial equation type (Equation 9) with residuals

The relative error calculus was used as tool for the comparison between the calculated data generated with the dynamic viscosity final equation and the existing tabular data (Table 9). The obtained results revealed a final average of 0.59% (absolute value) indicating a neglectable difference for the analyzed data.

The ANOVA analysis (Table 10) was used to compare the values of dynamic viscosity tabular and calculated data at 10 different concentrations in 4 temperatures variation. The results presented in Table 10 showed that the sample  $P$ -value is 0.9997 greater than the targeted alpha 0.05 and the  $F_{crit}$  value is larger than the  $F$ -test value. As presented in the case of citric acid density data the null hypothesis is not rejected indicating that is not a statistical difference between tabular and calculated data.

**Table 8.** Coefficients for equation no. 9

Coefficient	Value	Coefficient	Value
$a_1$	2803.9225	$a_4$	-0.014509371
$a_2$	-7.3756887	$a_5$	0.032140717
$a_3$	-19.001965	$a_6$	0.0052423574

**Table 9.** For dynamic viscosities of citric acid aqueous solutions the absolute value of relative errors for calculated data versus tabular data

Citric acid concentration, C [% w/w]	Dynamic viscosity, $\mu \cdot 10^3$ [Pa·s]											
	Temperature, T [K]											
	298.15		$\varepsilon$ , %	303.15		$\varepsilon$ , %	308.15		$\varepsilon$ , %	313.15		$\varepsilon$ , %
	TD*	CD*		TD	CD		TD	CD		TD	CD	
0	0.894	0.907	1.49	0.800	0.807	0.92	0.722	0.721	0.14	0.658	0.647	1.66
6.43	1.045	1.030	1.36	0.920	0.914	0.56	0.813	0.814	0.21	0.725	0.729	0.60
9.94	1.118	1.106	1.01	0.985	0.980	0.43	0.869	0.872	0.37	0.772	0.779	1.00
16.99	1.280	1.281	0.13	1.131	1.132	0.12	1.002	1.004	0.21	0.885	0.895	1.14
19.82	1.365	1.361	0.27	1.205	1.201	0.31	1.068	1.063	0.38	0.943	0.947	0.45
25.18	1.532	1.528	0.20	1.345	1.345	0.06	1.193	1.189	0.30	1.059	1.056	0.22
30.00	1.693	1.701	0.48	1.482	1.494	0.83	1.331	1.317	0.99	1.179	1.168	0.90
34.00	1.843	1.862	1.04	1.631	1.632	0.10	1.445	1.437	0.53	1.275	1.272	0.23
39.94	2.122	2.136	0.66	1.857	1.867	0.57	1.632	1.639	0.46	1.454	1.447	0.45
44.99	2.432	2.407	1.02	2.120	2.099	0.96	1.825	1.839	0.76	1.613	1.619	0.41
	Average $\varepsilon$ , %		0.76	Average $\varepsilon$ , %		0.48	Average $\varepsilon$ , %		0.43	Average $\varepsilon$ , %		0.70

\* TD – tabular data, CD – calculated data

**Table 10.** The ANOVA test summary

SUMMARY	Temperature, T [K]				Total	
	298.15	303.15	308.15	313.15		
<i>Tabular data</i>						
Count	10	10	10	10	40	
Sum	15.324	13.476	11.9	10.563	51.263	
Average	1.5324	1.3476	1.19	1.0563	1.281575	
Variance	0.243082	0.181768	0.133103	0.102487	0.184821	
<i>Calculated data</i>						
Count	10	10	10	10	40	
Sum	15.32305	13.47675	11.89911	10.56272	51.26163	
Average	1.532305	1.347675	1.189911	1.056272	1.281541	
Variance	0.2425	0.180038	0.134774	0.102028	0.184565	
ANOVA						
<i>Source of Variation</i>	<i>SS*</i>	<i>df*</i>	<i>MS*</i>	<i>F</i>	<i>P-value*</i>	<i>F crit</i>
Sample	2.34E-08	1	2.34E-08	1.42E-07	0.9997	3.973897
Columns	2.528057	3	0.842686	5.108037	0.002922	2.731807
Interaction	9.3E-08	3	3.1E-08	1.88E-07	1	2.731807
Within	11.87802	72	0.164973			

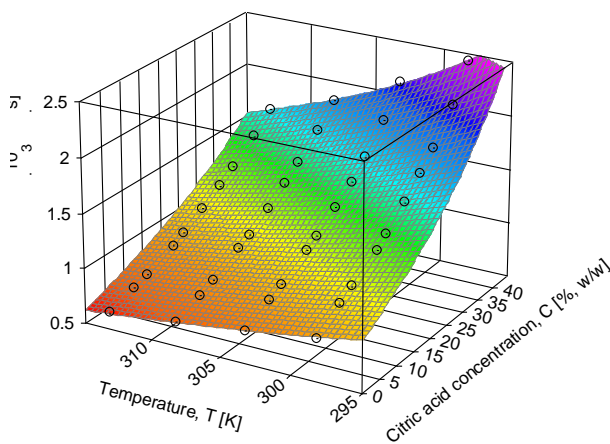
\* SS – sum of squares, df – degrees of freedom, MS – mean square, P-value – level of significance

**Table 11.** Coefficients for equation no. 11

Coefficient	Value	Coefficient	Value
$b_1$	-0.85692331	$b_4$	0.0004995215
$b_2$	-0.00043388783	$b_5$	-0.18401808
$b_3$	0.14271232		

By plotting directly the tabular data for the dynamic viscosity in TableCurve 3D® v.4 software an equation for the response surface was generated. The Equation 11 is a linear equation, Rank 5, Eqn. 1025 in TableCurve 3D® v.4 library with a precision of  $R^2 = 0.99950889$ ,  $\text{FitSdErr} = 0.01056894$ ,  $\text{Fstat.} = 17808.03$ . Its coefficients are presented in Table 11.

$$\mu = \frac{b_1 + b_2 \cdot C + b_3 \cdot \ln T}{1 + b_4 \cdot C + b_5 \cdot \ln T} \quad (11)$$



**Figure 3.** Citric acid aqueous solutions dynamic viscosity values plotted in TableCurve 3D and fitted with linear equation type (Equation 11) with residuals

Combining the models developed for the calculation of dynamic viscosity and density of citric acid aqueous solutions, the kinematic viscosity ( $\nu$ ) can be calculated using equation 12:

$$\nu = \frac{\mu}{\rho} [\text{m}^2 \cdot \text{s}^{-1}] \quad (12)$$

#### 4. CONCLUSIONS

The approach of the realized work led to mathematical relations with good adjustments to tabular existing data. For density two equations were formulated with average relative errors (absolute value) of 0.03% (Equation 4) and respectively  $R^2 = 0.9999$  and average relative errors (absolute value) of 0.01% (Equation 5) for intervals of temperature of 298.15 to 313.15 K and dry matter

concentration range between 6 to 45%. Dynamic viscosity variation is well described by an equation based on Arrhenius mathematical model with average relative errors of 0.59% (Equation 10) generated in the same range of temperature and citric acid concentration.

The proposed mathematical models can be loaded in the common or dedicated PC software and for targeted concentrations and temperatures the values of the studied thermophysical properties can be found easier and with a higher precision than using the existing experimental data in tabular form or graphic form. More if considering that for the tabular experimental data when values are not founded an inter- or extrapolation calculus is needed and for graphic form a software digital extraction of represented values is necessary.

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